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# Research Paper



# Persistent free radicals in biochar enhance superoxide-mediated Fe(III)/Fe (II) cycling and the efficacy of CaO<sub>2</sub> Fenton-like treatment

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#### ABSTRACT

Superoxide radicals  $(O_2^{\bullet^*})$  produced by the reaction of Fe(III) with  $H_2O_2$  can regenerate Fe(II) in Fenton-like reactions, and conditions that facilitate this function enhance Fenton treatment. Here, we developed an efficient Fenton-like system by using calcium peroxide/biochar (CaO<sub>2</sub>/BC) composites as oxidants and tartaric acid-chelated Fe(III) as catalysts, and tested it for enhanced  $O_2^{\bullet^*}$ -based Fe(II) regeneration and faster sulfamethoxazole (SMX) degradation. SMX degradation rates and peroxide utilization efficiencies were significantly higher with CaO<sub>2</sub>/BC than those with CaO<sub>2</sub> or  $H_2O_2$  lacking BC. The CaO<sub>2</sub>/BC system showed superior activity to reduce Fe(III), while kinetic analyses using chloroform as a  $O_2^{\bullet^*}$  probe inferred that the  $O_2^{\bullet^*}$  generation rate by CaO<sub>2</sub>/BC was one-half of that by CaO<sub>2</sub>. Apparently,  $O_2^{\bullet^*}$  is utilized more efficiently in this system to regenerate Fe(II) and enhance SMX degradation. Additionally, a positive correlation between SMX degradation rate constants and EPR signal intensities of biochar-derived persistent free radicals (PFRs) in CaO<sub>2</sub>/BC was obtained. We postulate that PFRs enhanced Fe(III) reduction by shuttling electrons donated by  $O_2^{\bullet^*}$ . This represents a new strategy to augment the ability of superoxide to accelerate Fe(III)/Fe(II) cycling for increased hydroxyl radical production and organic pollutant removal in Fenton-like reactions.

#### 1. Introduction

Fenton and Fenton-like systems are widely used to remove refractory organic contaminants in wastewater (Qin et al., 2015; Thomas et al., 2021) or soil (Yang et al., 2019) due to their effectiveness in producing reactive oxygen species (ROS) by using hydrogen peroxide (H2O2) and iron-based catalysts (Liu et al., 2021; Wang and Tang, 2021a). Among the various involved ROS, hydroxyl radicals (•OH) that are generated from the fast reduction of H<sub>2</sub>O<sub>2</sub> by Fe(II) (Eq. 1) (Pham et al., 2009) play a dominant role in organic oxidation (Wang et al., 2021b; Yang et al., 2018, 2021). However, this reaction oxidizes Fe(II) to Fe(III), and the subsequent regeneration of Fe(II) by H<sub>2</sub>O<sub>2</sub> is sluggish (Eq. 2) (Hou et al., 2017; Zhou et al., 2020; Zhu et al., 2020a), which greatly limits the efficiency of this advanced oxidation system. The simultaneously generated superoxide (O2 • ) is another important ROS (Eq. 2), which facilitates the reduction of Fe(III) (Eq. 3) (Li et al., 2016; Pan et al., 2018). However, due to the low yield and poor reactivity of  $O_2^{\bullet-}$  in water, slow Fe(III)/ Fe(II) cycling remains the bottleneck in Fenton based treatment technologies (Pignatello et al., 2006; Rose and Waite,

$$Fe^{2+} + H_2O_2 \rightarrow Fe^{3+} + \bullet OH + OH^-(k_1 = 76(\pm 1.9) \times 10^5 M^{-1}s^{-1})$$
 (1)

$$Fe^{3+} + H_2O_2 \rightarrow Fe^{2+} + HO_2^{\bullet}(O_2^{\bullet-}) + H^+(2H^+)(k_2 = 0.002 M^{-1}s^{-1})$$
 (2)

$$Fe^{3+} + O_2^{\bullet -} \rightarrow Fe^{2+} + O_2(k_3 = 10^7 \sim 10^8 \, M^{-1} s^{-1})$$
 (3)

Several strategies have been developed to promote  $O_2^{\bullet}$  production and accelerate Fe(II) regeneration and Fenton-like reactions (Huang et al., 2021). Metal ions, such as  $Mn^{2+}$ , can react with Fe (III)-nitrilotriacetic acid complexes and promote  $O_2^{\bullet}$  production in homogeneous systems (Li et al., 2016). Chelates like ethylenediamine-N, N'-disuccinic acid can serve as superoxide radical-promoting agents to enhance  $O_2^{\bullet}$  production (Huang et al., 2013; Rastogi et al., 2009). Metal peroxides (Xue et al., 2019) such as CaO<sub>2</sub> (Tang et al., 2020) and MgO<sub>2</sub> (Yuan et al., 2019; Zhu et al., 2020b) produce  $O_2^{\bullet}$  three orders of magnitude faster than  $H_2O_2$  due to their intrinsic reducibility. However, the increase of  $O_2^{\bullet}$  yield sacrifices the utilization efficiency of oxidants, because the superoxide radicals eventually convert into  $O_2$  by reducing

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<sup>2005;</sup> Xing et al., 2018).

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Fe(III) (Eq. 3) (Furman et al., 2009; Hayyan et al., 2016). Furthermore, superoxide is essentially unreactive in water due to the formation of hydrogen bonds and rapid disproportionation into  $O_2$  and  $H_2O_2$  (Furman et al., 2009). However, increasing the yield of  $O_2^{\bullet^-}$  should compensate for its low reactivity in water. Therefore, it is important to explore approaches to enhance the participation of  $O_2^{\bullet^-}$  to accelerate Fe (III) reduction (for faster Fe(III)/Fe(II) cycling) without decreasing utilization efficiency of peroxides.

Although aprotic solvents can effectively enhance  ${\rm O_2}^{\bullet^{\bullet}}$  reactivity by suppressing the formation of hydrogen bonds, there are very few reports about the enhancement of  ${\rm O_2}^{\bullet^{\bullet}}$  reactivity in water (Javed et al., 2020; Sawyer and Valentine, 1981; Smith et al., 2004). High  ${\rm H_2O_2}$  concentrations (> 0.3 M) that are frequently used in catalyzed  ${\rm H_2O_2}$  propagations in soil remediation can increase the production of  ${\rm O_2}^{\bullet^{\bullet}}$  (Mitchell et al., 2014). However, this approach is not feasible for water treatment because  ${\rm H_2O_2}$  at a high concentration can scavenge hydroxyl radicals and decrease the degradation efficiency of organic pollutants (Pignatello et al., 2006). Solid interfaces were reported to increase the reactivity of  ${\rm O_2}^{\bullet^{\bullet}}$  generated from KO<sub>2</sub>, and to facilitate hexachloroethane (HCA) degradation (Furman et al., 2009). However, these reactions are not Fenton-like, and the mechanism responsible for the enhanced reactivity of  ${\rm O_2}^{\bullet^{\bullet}}$  is unclear. Overall, modulating and increasing  ${\rm O_2}^{\bullet^{\bullet}}$  participation in Fenton-like reactions remains a significant technical challenge.

In this study, we used a CaO<sub>2</sub>-biochar system to enhance O<sub>2</sub>• utilization for improving Fe(III)/Fe(II) cycling in Fenton-like reactions. Biochar (BC) is a carbonaceous material obtained mainly from biomass pyrolysis (Sun et al., 2021), and has recently found wide applications in soil amendments (Liao et al., 2014), carbon storage (Sanchez et al., 2001), and heavy metal immobilization (Tian et al., 2019; Wang and Wang, 2019a). It is well-known that BC contains abundant persistent free radicals (PFRs) (Chen et al., 2020; Yang et al., 2016). These resonance-stabilized radicals, such as semiquinones and phenoxyls, serve as both electron donors and electron acceptors and participate in redox reactions (Klupfel et al., 2014; Yu et al., 2015; Zhong et al., 2019). However, there are very few reports on the influence of BC on the transformation and reactivity of ROS, which may be a missed opportunity for enhancing Fenton's reactions. In this work, we fabricated CaO2/BC based Fenton-like systems to enhance Fe(III)/Fe(II) cycling (and associated hydroxyl radical production) via superoxide-PFR interactions, and demonstrated the benefits of this novel approach for efficient sulfamethoxazole (SMX) degradation.

#### 2. Materials and methods

#### 2.1. Materials

All chemicals used and their sources are described in Supporting Information (Text S1). BC<sub>T</sub> was synthesized by calcining rice husk at different temperatures (T = 300, 400, 500 and 600 °C) according to previous procedures (Qin et al., 2016). Without specification, the BC in the oxidants was calcined at 400 °C.

#### 2.2. CaO2/BC preparation

CaO<sub>2</sub>/BC with different mass ratios of CaO<sub>2</sub> to BC was synthesized by using Ca(OH)<sub>2</sub> and H<sub>2</sub>O<sub>2</sub> as precursors (Li et al., 2020). Briefly, a given weight of BC was dispersed in 7 mL deionized water by magnetically stirring at 40 °C. Next, 2.5 g Ca(OH)<sub>2</sub> and 4.35 mL of H<sub>2</sub>O<sub>2</sub> (30 wt%) were successively added into the suspension. After magnetically stirring the mixture for 1 h, the powder was obtained by filtering, washing with ethanol, and drying at 30 °C for 12 h. The obtained materials were named as CaO<sub>2</sub>/BC-x (x = 1, 2, 4 and 6), where x represents the mass ratio of CaO<sub>2</sub> to BC. If not specified (without the label x), the mass ratio was 2 for CaO<sub>2</sub>/BC.

#### 2.3. SMX degradation in Fenton-like reactions

The performance of the Fenton-like reactions was assessed by the removal of the recalcitrant sulfonamide antibiotic, sulfamethoxazole (SMX). In a typical test, 1.2 mM tartaric acid (TA) and 0.6 mM Fe(NO<sub>3</sub>)<sub>3</sub> were added into 10 mg/L SMX solution (initial pH 7.0) in a 100 mL reactor under magnetic stirring (450 rpm) at 20 °C. The pH decreased to 2.6 after mixing for 20 min due to the addition of TA and the hydrolysis of Fe (III). CaO<sub>2</sub>/BC (1.2 mM peroxide dosage) was then added to initiate the reactions, and the final pH increased to 6.7 after 20 min due to the formation of Ca(OH)<sub>2</sub>.

A conventional Fenton reaction was also carried out (for benchmarking) using the same procedure, except that  $0.6 \text{ mM Fe}_2(\text{SO}_4)_3$  and  $1.2 \text{ mM H}_2\text{O}_2$  were used without addition of TA, and the pH was adjusted to  $2.6 \text{ with H}_2\text{SO}_4$  (1 M). Samples were withdrawn at a given interval, filtered and quenched by equal volumes of methanol. To evaluate the contribution of radicals, scavenging tests were carried out by using tertiary butanol (TBA) and chloroform as the scavengers of  $\bullet$ OH and  $\text{O}_2^{\bullet}$ , respectively. All experiments were performed in triplicate, and the results were reported as the mean values with standard deviations. Student's t-test was conducted to evaluate the significance of the differences between treatments at the 95% confidence level (p < 0.05).

#### 2.4. Analytical methods

The crystal phases of  $\text{CaO}_2$  and  $\text{CaO}_2/\text{BC}$  were examined on a Rigaku D/max-2200/PC X-Ray diffractometer (XRD). The surface functional groups were analyzed by a Fourier transform infrared spectrometer (FTIR, Nicolet 6700, Thermo, USA). The Raman spectra were measured on an inVia Qontor Raman spectrometer (Renishaw, Britain) with 532-nm excitation from a 25-mW He-Ne Laser. The morphologies of the samples were collected and observed on a field emission scanning electron microscope (FE-SEM, Nova NanoSEM 450, FEI). XPS analyses were performed on an Axis Ultra DLD system (Shimadzu/Kratos) of X-ray photoelectron spectroscopy (XPS).

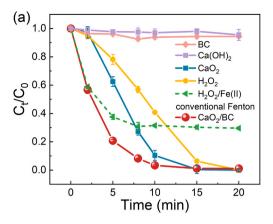
 $\rm H_2O_2$  concentrations were determined by a modified metavanadate method (Wei et al., 2021). The amount of peroxides in  $\rm CaO_2/BC$ -x and  $\rm CaO_2$  was measured by a potassium permanganate (KMnO<sub>4</sub>) titration method (Wu et al., 2019; Zhu et al., 2020b). The purity of these peroxide composites (which decreases with the presence of  $\rm Ca(OH)_2$ ) was determined based on the ratio of the measured peroxide content to the theoretical stoichiometric content.

The reactive oxygen species ( $\bullet$ OH,  $O_2^{\bullet}$  and  $^1O_2$ ) were detected by electron paramagnetic resonance (EPR) spectrometry (ELEXSYS E580, Bruker). The sweep field ranged from 3400 G to 3500 G, and microwave power and frequency were set at 15 mW and 9.67 GHz. 5,5-dimethyl-1pyrroline-N-oxide (DMPO) and 2,2,6,6-tetramethylpiperidine (TEMP) were used as the spin traps. The amount of dissolved ferrous ions was analyzed by a modified 1,10-phenanthroline chromogenic method. Quantitative analyses of residual SMX concentrations were performed on a high-performance liquid chromatography (HPLC, LC-20 CE, Shimadzu) equipped with a Shim Pack C18 chromatographic column (ZORBAX Eclipse XDBC18) and a UV-vis detector (SPD-20AV). The concentration of hexachloroethane (HCA) was determined on a Gas Chromatograph-Triple Quadrupole Tandem Mass Spectrometer (GCMS-QP2020, Shimadzu). The amount of total organic carbon (TOC) in the SMX degradation was determined by a TOC/TN analyzer (multi N/C 3100, Analytik Jena).

#### 3. Results and discussion

3.1.  $CaO_2/BC$  Fenton-like system efficiently utilizes peroxides to accelerate SMX degradation

SMX degradation was used to evaluate the performance of Fenton-like systems with various oxidants. Fig. 1(a) shows that BC or  $Ca(OH)_2$ 



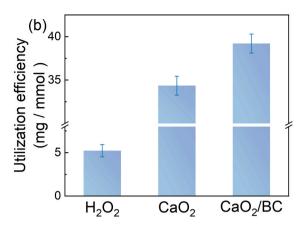


Fig. 1. (a) SMX degradation and (b) peroxide utilization efficiency in different reaction systems. All reactions contained  $[SMX]_0 = 10 \text{ mg/L}$ , [Fe(III)] = 0.6 mM,  $n_{Fe}$ :  $n_{TA} = 1.2$ , [BC] = 64 mg/L and [Peroxides] = 1.2 mM. The initial pH of the SMX solution was 7.0; this decreased to pH 2.6 after the addition of Fe(III)-TA, and increased to final pH 6.7; no TA was added in the conventional Fenton system.

(the hydrolysis product of CaO2) alone removed less than 5% SMX in 20 min, indicating that SMX adsorption on BC or Ca(OH)2 was minor. The systems with oxidants (H2O2 and/or CaO2) showed faster SMX removal (Fig. 1a). TA was used as the complexing agent to stabilize iron over a wide pH range and prevent its precipitation when the pH increased to 6.7 during the reaction (due to Ca(OH)2 production). SMX degradation in these systems was fitted by a pseudo-first-order kinetic model. The observed reaction rate constant  $(k_{obs})$  of the  $H_2O_2$ -based system was 0.17 ( $\pm$  0.007) min<sup>-1</sup>. This value was 0.22 ( $\pm$  0.003) min<sup>-1</sup> in the CaO<sub>2</sub> system, and SMX removal efficiency reached 99% at 15 min. The better performance of CaO<sub>2</sub>-based Fenton-like reactions is ascribed to the enhanced yield of superoxide radicals, which promotes the recycling of Fe(III) to Fe(II) (Pan et al., 2018; Wang et al., 2016). In contrast, the conventional Fenton system (Fe(II)/H2O2) resulted in fast initial SMX degradation rate (0.19  $\pm$  0.013 min<sup>-1</sup>, first 5 min) due to the prompt H<sub>2</sub>O<sub>2</sub> decomposition and •OH production, but the SMX degradation rate was very slow after 8 min and about 37% of SMX (10 mg/L initially) remained in the system (Fig. 1a). This can be attributed to Fe(III) accumulation and sluggish Fe(II) regeneration.

The synthesized CaO<sub>2</sub>/BC system has the highest SMX degradation rate coefficient (0.34  $\pm$  0.014 min<sup>-1</sup>), which was 1.5 times that of the CaO2 system without BC and 1.7 times higher than the traditional Fenton system. By using the CaO<sub>2</sub>/BC composite as the oxidant, SMX removal efficiency reached 96% at 10 min. As a control, a mixture made by adding BC powder into the CaO2 system to create a hybrid system (h-CaO<sub>2</sub>/BC) was tested; this slightly increased the  $k_{obs}$  to 0.24 ( $\pm$  0.013) min<sup>-1</sup>, about 9% more than the CaO<sub>2</sub> system without BC (Fig. S1a). The results indicate that the close contact between BC and CaO2 favors electron transfer and promotes the Fenton-like oxidation of SMX. Furthermore, in the absence of iron, the direct interaction between BC and H<sub>2</sub>O<sub>2</sub> did not induce significant SMX degradation in 20 min (Fig. S1b), indicating that the contribution of H<sub>2</sub>O<sub>2</sub> activation by BC was negligible for SMX degradation. These experiments show that the presence of BC effectively accelerated SMX degradation in the CaO2/BC Fenton-like reactions, significantly outperforming the controls and the traditional Fenton treatment (Fig. 1a). Adding BC powder to the H<sub>2</sub>O<sub>2</sub>/ Fe(III) system slightly increased  $k_{obs}$  from 0.17 ( $\pm$  0.007) to 0.19  $(\pm 0.0053) \text{ min}^{-1}$  (Fig. S2), suggesting its potential to also enhance conventional Fenton treatment.

The utilization efficiency of peroxides, that is, the total removed TOC per consumed peroxides, in various Fenton-like systems was estimated by measuring the residual  $\rm H_2O_2$  and TOC. The utilization efficiency (at the 20th min) for the  $\rm H_2O_2$  system (in terms of dissolved TOC removal) was only 5 mg-TOC per mmol peroxides (Fig. 1b and Fig. S3). The poor performance may be attributed to disproportionation of  $\rm H_2O_2$  and low mineralization of organics. In contrast, the utilization efficiencies of the

 $CaO_2$  and  $CaO_2/BC$  systems were significantly improved, reaching 34 and 39 mg TOC removed/mmol peroxides, respectively. The peroxide utilization efficiency was also evaluated based on SMX removal, and was significantly higher for the  $CaO_2/BC$  system than for the systems with  $H_2O_2$  or  $CaO_2$  alone (i.e., 52.6 vs. 12.1 and 12.6 mg-SMX/mmol peroxides, respectively, Fig. S4). These results imply that the peroxides utilization efficiency is much higher for  $CaO_2$  than for  $H_2O_2$ , and the incorporation of BC can simultaneously accelerate SMX degradation and improve the peroxide utilization efficiency.

The effect of mass ratios of  $\text{CaO}_2$  to BC on SMX degradation was investigated while holding constant the peroxide concentration in each reaction (Fig. 2a). SMX removal was accelerated with increasing BC content, up to 100% removal in 15 min. However, the  $\text{CaO}_2/\text{BC-2}$  and  $\text{CaO}_2/\text{BC-4}$  systems showed similar kinetics of SMX degradation, achieving 97% SMX removal in 8 min. Further increasing the BC content to 50% (composite  $\text{CaO}_2/\text{BC-1}$ ) resulted in a decreased SMX removal efficiency, since too much BC apparently inhibits ROS generation. The purity (in terms of peroxide content) of the composite oxidants increased with increasing BC content (Fig. 2b), which may be due to BC facilitating uniform dispersion of  $\text{Ca}(\text{OH})_2$  and its transformation to  $\text{CaO}_2$ . The first-rate constants (k) were shown in Fig. 2(b), in which  $\text{CaO}_2/\text{BC-2}$  exhibited the highest k value (0.34  $\pm$  0.014 min $^{-1}$ ). Thus,  $\text{CaO}_2/\text{BC-2}$  was selected for further tests.

The compositions and structures of the optimized CaO2/BC were explored. Raman spectroscopy showed a strong peak for CaO2/BC at 845 cm<sup>-1</sup> (Fig. 2c), corresponding to the expected O-O stretching vibration in CaO<sub>2</sub> (Wu et al., 2018). However, the peak slightly positively shifted compared to that of CaO<sub>2</sub> (843 cm<sup>-1</sup>), which can be attributed to that the chemical environment of peroxide bonds changed after the incorporation of BC (Guo et al., 2015). In the FTIR spectra, the absorption bands at 875 cm<sup>-1</sup> were attributed to the O–O bridge of CaO<sub>2</sub> (Fig. S5a) (Zeglinski et al., 2006), and the two peaks at 1410 and 1490 cm<sup>-1</sup> were ascribed to O-Ca-O bending vibrations (Yan et al., 2009). The band corresponding to the stretching vibration of C-O-C in BC, located at  $1051 \text{ cm}^{-1}$ , shifted to  $1076 \text{ cm}^{-1}$  in the spectrum of CaO2/BC; this indicates a strong interaction between CaO2 and BC, which facilitates interactions between the released ROS and proximal BC (Li et al., 2020). The XRD patterns suggest that tetragonal-phase CaO<sub>2</sub> (JCPDS Card 85-514) is formed in the CaO<sub>2</sub>/BC composites (Fig. S5b) (Wang et al., 2019b). The morphology of BC and CaO2/BC was characterized by SEM (Fig. S5c and d). BC had a porous structure, while CaO2/BC exhibited spherical CaO2 particles dispersed on the surface of BC. There was agglomeration of CaO<sub>2</sub> particles due to their high surface energy (Wu et al., 2019). The strong peak at g = 2.0021 in the EPR spectra of BC proved the existence of PFRs. The peak shifted to g = 2.0037 for CaO<sub>2</sub>/BC (Fig. 2d), which may be attributed to the

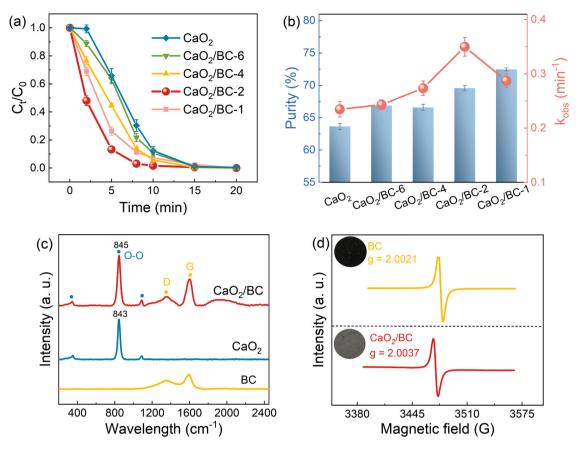


Fig. 2. The effect of mass ratios of CaO<sub>2</sub> to BC on (a) SMX degradation (CaO<sub>2</sub>/BC-x, where x is the mass ratio of CaO<sub>2</sub> to BC, and as x decreases so does the proportion of CaO<sub>2</sub>) and (b) peroxide purity and SMX degradation rate constants; (c) Raman spectra of CaO<sub>2</sub>/BC, CaO<sub>2</sub> and BC; (d) EPR spectra of CaO<sub>2</sub>/BC and BC ([SMX]<sub>0</sub> = 10 mg/L, [Fe(III)] = 0.6 mM,  $n_{Fe}$ : $n_{TA}$  = 1:2, [BC] = 64 mg/L, [peroxides] = 1.2 mM).

transformation of PFRs from carbon centered types into carbon-oxygen centered types due to the incorporation of peroxides (Xin et al., 2021; Zhong et al., 2018). These data show that a  $CaO_2$  and BC composite with a significant amount of PFRs was obtained.

The effects of the molecular ratio of Fe(III) to TA ( $R_{Fe/TA}$ ), total iron concentrations, oxidant dosages, and initial pH on SMX degradation in the CaO<sub>2</sub>/BC systems were investigated (Fig. S6). The optimal  $R_{Fe/TA}$  and iron concentration were 1:2 and 0.6 mM, respectively. Significant SMX degradation was achieved at a wide initial pH range (from 3.0 to 10.0). This could be attributed to TA serving as the chelator to stabilize Fe(III). Excess TA exerts steric hindrance on Fe<sup>2+</sup>, hindering the reaction

between the complex and  $\rm H_2O_2$  generated by  $\rm CaO_2/BC$  (Tang et al., 2020). SMX removal efficiency increased with increasing  $\rm CaO_2/BC$  dosage from 0.4 to 1.2 mM, but was strongly inhibited with further increases in oxidant content since excess  $\rm CaO_2/BC$  increased the slurry's pH (to about pH 11.3 at 2.0 mM peroxides) (Tang et al., 2020; Yan et al., 2021). Significant SMX degradation was achieved at a wide initial pH range (from 3.0 to 10.0), which could be attributed to TA chelating and stabilizing Fe(III). Overall, the  $\rm CaO_2/BC$  system shows satisfactory activity at a wide range of pH values, enhancing its utility for application in a wide range of environments.

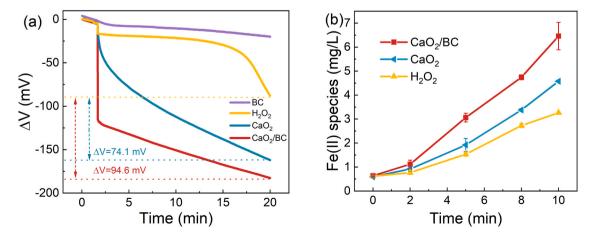


Fig. 3. (a) Changes of open circuit potentials of Pt electrodes and (b) dissolved Fe(II) in different Fenton-like systems ([SMX] $_0 = 10 \text{ mg/L}$ , [Fe(III)] = 0.6 mM,  $n_{Fe}$ :  $n_{TA} = 1:2$ , [BC] = 64 mg/L, [peroxides] = 1.2 mM).

#### 3.2. The CaO<sub>2</sub>/BC system enhanced Fe(II) regeneration

In Fenton-like systems, reductants such as superoxide are important to regenerate Fe(II) and subsequently produce hydroxyl radicals. Reduction activity in each Fenton-like system was evaluated by measuring the changes of open-circuit potentials ( $\Delta V$ ) at the Pt electrode. The  $\Delta V$  value was relatively constant in the BC alone system and declined immediately with the addition of all oxidants (Fig. 3a), suggesting the decrease of redox potentials in the systems. This can be attributed to the generation of reducing constituents such as Fe(II) and superoxide radicals (Barreiro et al., 2007; Chen et al., 2002; Pan et al., 2018). The trend of the Fenton-like systems with a greater  $\Delta V$  was consistent with that of SMX degradation efficiencies in the corresponding systems. The decreased open-circuit potentials at the 20th min in CaO<sub>2</sub> and CaO<sub>2</sub>/BC systems are 74.1 mV and 94.6 mV more than that of the H<sub>2</sub>O<sub>2</sub> system, respectively. This suggests that more reductive substances are generated in both CaO2 containing systems, and that BC promotes the generation of reductive substances in the reactions. The  $\Delta V$  values in the absence of the chelating agent (TA) were also measured (Fig. S7). The order of  $\Delta V$  in the absence of TA is the same as that in the presence of TA, revealing that BC was critical for the increased reduction potentials and promoted SMX oxidation.

The concentration of Fe(II) in each system was compared to show the enhanced generation of reductive substances in the Fenton-like reactions (Fig. 3b). Fe(II) concentrations increased as the reaction progressed; the CaO<sub>2</sub>/BC system had the highest concentration of Fe(II), followed by the CaO2 and H2O2 systems. The results are consistent with the open-circuit potential measurements. It is known that BC has the potential to directly reduce Fe(III) due to its ability to serve as an electron donor that has a capacity in the range of 0.24-1.83 mmol electrons/ g (Chacón et al., 2020; Xu et al., 2020; Zhang et al., 2018). However, the actual contribution of BC alone to the generation of Fe(II) is negligible, and the reduction kinetics by BC-only control systems are sluggish (Fig. S8). The final concentrations of Fe(II) at 10 min in the presence of BC or BC and TA were only 0.09 mg/L and 0.61 mg/L, much lower than that observed in the CaO<sub>2</sub>/BC Fenton-like system (6.45 mg/L), which may be due to the low reduction potential of electrons in BC. Thus, Fe(II) generation was promoted by the presence of BC in the CaO<sub>2</sub>/BC system, which subsequently favors hydroxyl radical production and SMX degradation (Fig. 1a).

# 3.3. Higher superoxide reactivity in the $CaO_2/BC$ system was a critical enhancing factor

Although  $\bullet \mathrm{OH}$  is the main ROS responsible for treatment in Fenton-

like systems,  $O_2^{\bullet \bullet}$  played a significant indirect role in enhancing  $\bullet$ OH production and SMX treatment, as detailed below. The main ROS contributing to SMX degradation in the CaO<sub>2</sub> and CaO<sub>2</sub>/BC systems were evaluated by EPR analysis and scavenging tests. In the EPR spectra, the characteristic four peaks with an intensity ratio of 1:2:2:1 for the hydroxyl-radical adduct DMPO-OH were observed in both the CaO<sub>2</sub> and CaO<sub>2</sub>/BC systems (Fig. 4a inset and Fig. S9) (Han et al., 2014; Qin et al., 2021). Fig. 4(a) compares the signal intensities of DMPO-OH adducts in the two systems at different times, and corroborates that the CaO<sub>2</sub>/BC system produced significantly higher concentrations of  $\bullet$ OH (p < 0.05) to facilitate SMX degradation. Furthermore, tertbutyl alcohol (TBA) was used to scavenge hydroxyl radicals ( $k_{\bullet OH/TBA} = 6.0 \times 10^8 \, M^{-1} s^{-1}$ ) (Buxton et al., 1988). SMX degradation was almost completely inhibited in the presence of TBA, corroborating the critical role of  $\bullet$ OH in both treatment systems (Fig. 4b).

The characteristic six peaks for the superoxide-radical adduct DMPO-OOH were observed in both the CaO<sub>2</sub> and CaO<sub>2</sub>/BC systems (Fig. S10). With the addition of 10 mM chloroform as the scavenger of superoxide radicals  $(k_{O_2^{*-}/chloroform}=3.0\times10^{10}~M^{-1}s^{-1})$  (Buxton et al., 1988), the SMX degradation rate constant for the CaO<sub>2</sub> system (Fig. 4b) decreased by 80% (from  $0.22\pm0.003-0.048\pm0.003~min^{-1}$ ), while that for CaO<sub>2</sub>/BC decreased more significantly by 96% (from  $0.34\pm0.014-0.014\pm0.001~min^{-1}$ ). This indicates that superoxide radicals contribute to the CaO<sub>2</sub>/BC system's higher treatment efficiency.

While scavenger tests indicate that hydroxyl radical is the most important radical contributing to SMX degradation (Fig. 4b and Fig. S11), superoxide clearly plays a significant role as a reductant in the enhanced degradation mechanism of the CaO<sub>2</sub>/BC system. The importance of O<sub>2</sub>• in this treatment system was demonstrated by using various concentrations of chloroform, which serves as a probe that reacts with O<sub>2</sub>• (Huang et al., 2013; Pan et al., 2018). As shown in Fig. 5(a) and Fig. S12a, SMX removal efficiencies for both CaO<sub>2</sub> and CaO<sub>2</sub>/BC systems were progressively inhibited as chloroform concentrations (and thus superoxide scavenging) increased. Note that the relationship between the initial SMX degradation rates ( $R_{SMX}^d M \bullet s^{-1}$ ) and chloroform dosages was well fitted by a hyperbolic function (Eq. 4).

$$R^{d}_{SMX} = \frac{R^{f}_{O_{2}^{\bullet-}} \times k_{SMX,O_{2}^{\bullet-}} \times c_{SMX}}{k_{chloroform,O_{2}^{\bullet-}} \times c_{chloroform} + k_{SMX,O_{2}^{\bullet-}} \times c_{SMX} + k_{Fe^{III}-TA,O_{2}^{\bullet-}} \times c_{Fe^{III}-TA}}$$

$$(4)$$

where,  $R_{O_2^-}^f$  is the formation rate of  $O_2^-$  ( $Ms^{-1}$ ), and  $k_{SMX,O_2^{--}}$ ,  $k_{chloroform,O_2^-}$ , and  $k_{Fe^{III}-TA,O_2^-}$  are second-order rate constants of superoxide radicals reacting with SMX, chloroform, or  $Fe^{III}-TA$ ,

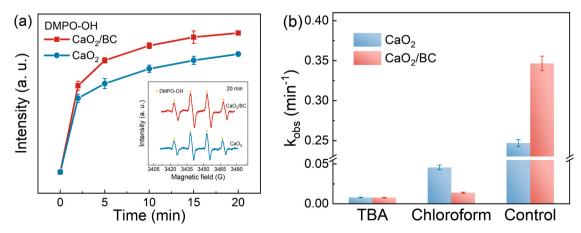


Fig. 4. (a) EPR signal intensity over time of DMPO-OH (hydroxyl radical adduct) in  $CaO_2/BC$  and  $CaO_2$  system (inset shows EPR signals of DMPO-OH at 20 min); (b) Effect of scavengers on SMX degradation in various systems ([SMX] $_0 = 10 \text{ mg/L}$ , [Fe(III)] = 0.6 mM,  $n_{Fe}$ :  $n_{TA} = 1:2$ , [peroxides] = 1.2 mM, [TBA] = 10 mM, [chloroform] = 10 mM).

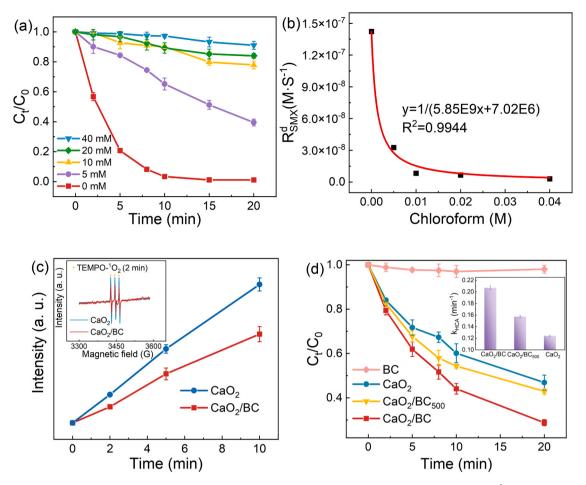


Fig. 5. (a) Effect of chloroform concentration on SMX degradation in  $CaO_2/BC$  system; (b) initial degradation rate of SMX ( $R_{SMX}^d$ ) as a function of chloroform concentrations in  $CaO_2/BC$  system; (c) the evolution of signal intensities of TEMPO- $^1O_2$  adducts in the presence of 10 mM TBA and (d) HCA degradation in the  $CaO_2$  and  $CaO_2/BC$  systems ([SMX] $_0 = 10$  mg/L, [HCA] $_0 = 500$  µg/L, [Fe(III)] = 0.6 mM,  $n_{Fe}$ : $n_{TA} = 1$ :2, [peroxides] = 1.2 mM, pH $_0 = 7$ .0). Inset in (c) is the TEMP- $^1O_2$  signals at 2 min, and that in (d) is the HCA degradation rate constants in different systems.

respectively. The  $R_{O_2^+}^f$  in the CaO<sub>2</sub> and CaO<sub>2</sub>/BC systems can be calculated by Eq. (5) based on the fitting parameter a (Huang et al., 2013; Pan et al., 2018).

$$R_{O_2^{\bullet-}}^f = \frac{k_{chloroform,O_2^{\bullet-}}}{a \times k_{SMX,O_2^{\bullet-}} \times c_{SMX}}$$
(5)

Although the value of  $k_{SMX,O_2^{\bullet-}}$  is unknown, the ratio of the two  $R_{O_2^{\bullet-}}^f$ values for the CaO<sub>2</sub>/BC (Fig. 5b) and CaO<sub>2</sub> (Fig. S12b) systems can be obtained from the inverse ratio of parameter a (Text S3). Surprisingly,  $R_{O_2^{+-}}^f$  in the CaO<sub>2</sub> system was 2.1 times that of the CaO<sub>2</sub>/BC system. Control tests indicated that the difference in H2O2 release from CaO2 versus CaO2/BC systems was negligible during the first 30 min (Fig. S13). These results unequivocally demonstrate that the presence of BC decreases the yield of  $O_2^{\bullet}$  from CaO<sub>2</sub>. This may be explained by the fact that the CaO2/BC system produces more ferrous species (Fig. 3b), which promote the conversion of peroxides into hydroxyl radicals (Eq. 1) and simultaneously decrease reaction rates between peroxides and ferric ions (Eq. 2) that produce superoxide. The decreased O2 • yield by incorporating BC is also consistent with the results on the enhanced utilization efficiency of peroxides in CaO2, because less O2. production can avoid the consumption of peroxides through a reductive pathway. Taken together, these results indicate that  $O_2^{\bullet-}$  produced by the CaO<sub>2</sub>/ BC system is more efficiently used to reduce Fe(III) to Fe(II) (and thus enhance •OH production) compared to the CaO<sub>2</sub> control.

Lower  $O_2^{\bullet}$  production in the CaO<sub>2</sub>/BC system compared to controls

was corroborated by the detection of  $^1O_2$  using EPR spectroscopy. In Fenton-like reactions,  $^1O_2$  can be produced by  $O_2^{\bullet^-}$  disproportionation (Eq. 6,  $k=2.4\times 10^{12-pH}\,M^{-1}s^{-1}$ ) (Wang et al., 2020). Since  $\bullet$ OH can increase the generation of  $^1O_2$  by participating a series of radical reactions (Yi et al., 2019; Dou et al., 2019), the experiments were conducted in the presence of TBA, a hydroxyl radical scavenger. Under these conditions of suppressed  $\bullet$ OH generation, the produced  $^1O_2$  is positively correlated with the amount of  $O_2^{\bullet^-}$  produced (Nosaka and Nosaka, 2017; Ali et al., 2020).

$$2O_2^{\bullet -} + 2H_2O \to {}^{1}O_2 + H_2O_2 + 2HO^{-}$$
(6)

The EPR signal intensities of TEMPO- $^1O_2$  in the CaO $_2$  and CaO $_2$ /BC systems were detected. The three typical peaks with an intensity ratio of 1:1:1 in both EPR spectra correspond to the spin adduct of TEMPO- $^1O_2$  (Duan et al., 2018; Miao et al., 2020). The intensity of TEMPO- $^1O_2$  in the CaO $_2$  system is obviously higher than that of the CaO $_2$ /BC system at 2 min (inset in Fig. 5c), demonstrating a higher concentration of  $^1O_2$  in the CaO $_2$  system without BC. The evolution of  $^1O_2$  concentration in the first 10 min was also monitored (Fig. 5c). When using CaO $_2$ /BC as the oxidant, the generation of  $^1O_2$  remained lower than that of the CaO $_2$  system within 10 min, which confirms that the presence of BC decreased the production of  $O_2$ . Interestingly, even though the CaO $_2$ /BC system produced less  $O_2$ . it recycled Fe(II) faster (Fig. 3b), produced more  $\bullet$ OH (Fig. 4a), and (consistently) degraded SMX faster (Fig. 1a). This indicates that  $O_2$ . reactivity is enhanced by BC in the CaO $_2$ /BC Fenton-like reactions, contributing to increased SMX removal.

Enhanced O2 er reactivity with CaO2/BC can be further shown by

hexachloroethane (HCA) degradation tests, because HCA is susceptible to reduction by  ${\rm O_2}^{\bullet}$  but not to oxidation by  ${\bullet}$ OH (Furman et al., 2009). Only about 2% HCA was removed in the BC alone system (Fig. 5d), indicating that HCA adsorption on BC was minor. The CaO<sub>2</sub>/BC based system exhibits a much higher HCA removal efficiency, reaching 71.2% in 20 min. The rate constant of the CaO<sub>2</sub>/BC system ( $k_{HCA}=0.2\pm0.003~{\rm min}^{-1}$ ) was approximately two times higher than that of the CaO<sub>2</sub> system ( $k_{HCA}=0.12\pm0.015~{\rm min}^{-1}$ ), even though superoxide production in the CaO<sub>2</sub>/BC system was lower. These results confirm that the CaO<sub>2</sub>/BC system enhances the reactivity of O<sub>2</sub> $^{\bullet}$ .

#### 3.4. PFRs in BC promote electron transfer from superoxide to Fe(III)

To explore the critical constituents of BC that enhance  $O_2^{\bullet-}$  reactivity, BC with different contents of PFRs were synthesized by calcining rice husk at various temperatures. A series of CaO<sub>2</sub>/BC<sub>T</sub> ("T" = calcination temperature in °C) were obtained by using the BC<sub>T</sub> as the precursors. PFR content in the CaO<sub>2</sub>/BC<sub>T</sub> samples can be represented by the EPR intensities. The EPR spectra of the composite oxidants showed that the PFR content is variable (Fig. S14a), and that BC calcined at 400 °C had the highest signal intensity and PFR content, which is consistent with previous reports (Fang et al., 2015). The oxidants were used in SMX degradation tests at the same peroxide dosages (Fig. S14b), and apparent reaction rate constants were obtained. A positive linear correlation between SMX degradation rate constants and PFR content was observed (Fig. 6a). SMX degradation was faster with higher PFR content, which facilitated electron transfer from O2 to Fe(III) in Fe-TA complexes, and accordingly promoted Fenton-like reactions. The significant contribution of PFRs to  $O_2^{\bullet-}$  participation is corroborated by lower HCA degradation activity in the CaO<sub>2</sub>/BC<sub>500</sub> system (Fig. 5d), in which the intensity of PFRs was about one-half of those in CaO2/BC, indicating lower  $O_2^{\bullet}$  availability in a system with lower PFR content.

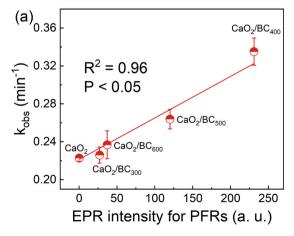
PFRs in BC<sub>400</sub> were reduced by pre-treating BC with 30 wt%  $\rm H_2O_2$  for 40 h to partially eliminate the surface PFRs (Liu et al., 2020; Zhao et al., 2018). A composite labeled as  $\rm CaO_2/BC_d$  was synthesized from the treated BC with depleted PFRs. According to the EPR spectra (inset in Fig. 6b), the signal intensity of PFRs in the  $\rm CaO_2/BC_d$  was reduced after  $\rm H_2O_2$  treatment. Simultaneously, the SMX degradation performance of  $\rm CaO_2/BC_d$  was much poorer than that of the untreated  $\rm CaO_2/BC$ , and the  $\rm k_{obs}$  values decreased from 0.34 ( $\pm$  0.014) to 0.22 ( $\pm$  0.024) min<sup>-1</sup>. The EPR signal intensity of PFRs decreased in the  $\rm CaO_2/BC$  system after the reaction, while changes in the BC-alone system were negligible (Fig. S15). This indicates the involvement (and consumption) of PFRs in the  $\rm CaO_2/BC$  treatment systems, where PFR content in BC would influence  $\rm O_2^{\bullet c}$  reactivity towards Fe(II) regeneration (see graphical abstract).

Surface-associated chemical species on fresh and used  $CaO_2/BC$  samples were investigated by XPS analyses. The C 1s spectra (Fig. S16) were fitted into three peaks at 284.98 eV, 286.10 eV and 289.02 eV, corresponding to C–C, C–O and C=O, respectively (Ali et al., 2021). The binding energy of C=O decreased from 289.02 to 288.73 eV after reaction, and its percentage increased from 18% to 24%. This suggests that the PFRs were involved in SMX degradation by facilitating electron transfer from carbon related groups on the surface of BC to Fe(III) (Yang et al., 2018). Based on the Fe 2p spectra (Fig. S17), Fe(II) and Fe(III) contents were 54% and 46%, respectively, in the residual  $CaO_2/BC$  sample, reflecting the recycling of Fe(III) to Fe(II) on the surface of BC (Zhou et al., 2020). Thus, the XPS results corroborate that PFRs on the surface of BC facilitate Fe(II) regeneration to enhance the efficacy of  $CaO_2$  Fenton-like treatment (see graphical abstract).

Overall, superoxide generated from CaO<sub>2</sub> can interact with PFRs, which are known to serve as electron shuttles and can reduce Fe(III) to regenerate critical Fe(II). Among the diverse types of PFRs in BC, the prevalent electron-accepting moieties, like semiquinone-types, can react with superoxide at a high reaction rate to form quinoid structures (Samoilova et al., 2011; Zhong et al., 2019). Subsequently, the quinoid reverse to semiquinone-types by reducing Fe(III). The disproportionation of O<sub>2</sub>• can be suppressed by binding on PFRs, and the PFRs facilitate electron transfer from superoxide to surface adsorbed Fe(III). Therefore, PFRs in BC facilitate the surface cycling of Fe(III)/Fe(II), and thus indirectly enhance the formation of •OH for pollutant decomposition. Overall, these results demonstrate the superior performance of the CaO<sub>2</sub>/BC Fenton-like system compared to BC-lacking controls and a traditional Fenton system, as it has both a high SMX degradation rate and peroxide utilization efficiency.

#### 4. Conclusion

Compared to traditional Fenton treatment and  $CaO_2$ -only and  $H_2O_2$ -only Fenton-like reactions without BC, the  $CaO_2/BC$  system showed enhanced removal of SMX and improved utilization efficiency of peroxides. The performance of  $CaO_2/BC$  Fenton-like reactions was correlated with the PFR content in BC. It was demonstrated that the direct interaction between BC and Fe(III) or  $H_2O_2$  to regenerate Fe(II) is sluggish and negligible. However, PFRs serve as electron shuttles to increase the ability of superoxide radicals to regenerate Fe(II) in the  $CaO_2/BC$  system, and accordingly promote the generation of hydroxyl radicals in Fenton-like reactions (as illustrated in the graphical abstract) even at circum-neutral pH. The enhanced participation of superoxide can also mitigate the unproductive consumption of peroxides to produce molecular oxygen, as well as augment the generation of hydroxyl



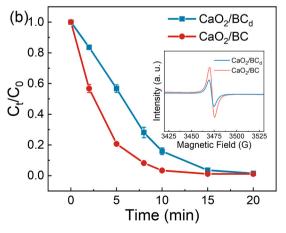


Fig. 6. Importance of persistent free radicals (PFR) in biochar. (a) Correlation between SMX degradation rate constants and the EPR signal intensity for different composites; (b) The decrease of SMX degradation by using the composite with the depleted BC, inset is the EPR spectra showing PFR signal intensity for CaO<sub>2</sub>/BC and CaO<sub>2</sub>/BC<sub>d</sub> (CaO<sub>2</sub>/BC<sub>d</sub> is obtained from the BC with depleted PFRs, [SMX] $_0 = 10 \text{ mg/L}$ , [Fe(III)] = 0.6 mM,  $_{R_E}$ : $_{R_E}$ 

radicals. This provides a novel strategy to enhance the utilization efficiency of both peroxides and superoxide radicals by combining PFRs in BC and solid metal peroxides, and offers mechanistic insight to accelerate the rate-limiting Fe(III) reduction in Fenton-like reactions.

Although  $\text{CaO}_2$  is not a common oxidant in Fenton-like reactions, it has great potential to mitigate logistical challenges associated with storage and transportation of the more commonly used  $\text{H}_2\text{O}_2$ . Furthermore,  $\text{CaO}_2$ -based Fenton-like reactions have superior performance over  $\text{H}_2\text{O}_2$ -based systems at circum-neutral pH. The proposed approach to enhance the participation of superoxide radicals by PFRs in biochar would enhance  $\text{CaO}_2$ -based Fenton-like reactions to efficiently remove recalcitrant organic contaminants in water treatment or soil remediation efforts.

#### CRediT authorship contribution statement

Shuqi Zhang: Data curation, Methodology, Investigation, Visualization, Writing – original draft. Yan Wei: Methodology, Investigation, Visualization. Jordin Metz: Visualization, Validation, Writing – review & editing. Shengbing He: Resources, Investigation. Pedro J. J. Alvarez: Resources, Validation, Writing – review & editing. Mingce Long: Conceptualization, Supervision, Funding acquisition, Resources, Writing – review & editing.

#### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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#### Appendix A. Supplementary data

The detailed information about materials and their sources; GC/MS analysis of HCA; method for dissolved Fe(II) detection; kinetic analysis of superoxide formation rates; FTIR, XRD, SEM and XPS analysis of samples; SMX degradation, release of  $H_2O_2$ , TOC removal, open-circuit potential curves, quenching tests, EPR spectra measurements of  $\bullet$ OH,  $O_2^{\bullet \bullet}$  and PFRs in different systems.

### Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.jhazmat.2021.126805.

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